

# Hydrodynamic Flow Past A Semi- Infinite Rough Plate Embedded In Porous Medium

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*Abstract:-* The boundary layer flow of a fluid past a semi-infinite rough plate embedded in porous medium is investigated. The transformed non-linear ordinary differential equation describing the problem is solved numerically using the shooting technique. The effects of permeability parameter ( $M$ ), inertia coefficient parameter ( $N$ ) and the roughness parameter ( $R_w$ ) on the velocity are shown on graphs. Numerical data for the skin fraction have been tabulated for various values of  $M, N$  and  $R_w$ .

*Key-Words:-* MHD, Flow, Porous, numerical solution, semi-infinite

## 1- Introduction

The analysis of hydrodynamic flow through porous medium is of interest in a wide range of technical problems. The importance of inertia effects were discussed by many authors [1-4].

In the a forementioned studies, the plates were asumed to be smooth. In most practical application connected with the flat plate, the wall can not be considered smooth. Consequently the flow past a rough plate is of as much practical interest [6].

To the end of our knowledge there have been no studies concerning the laminar boundary layer flow past a rough surfaces through a non-Darcian porous medium.

It is now proposed to study the effects of permeability parameter, inertia coefficient parameter and the roughness parameter on the flow past a semi-infinite plate embedded in non-Darcian porous medium.

## 2- Basic Equations

The boundary layer steady flow of an incompressible fluid through a porous medium bounded by a semi- infinite rough flat plate is

studied. The  $x$ -axis is taken along the plate and  $y$ -axis normal to it. We assume that:

- (a) the magnitude of the free-stream velocity is maintained and the flow is steady and two-dimensional;
- (b) the boundary-layer approximations hold;
- (c) the physical properties are constant; and
- (d) the velocity at the plate is proportional to the gradient of velocity.

Under these assumptions the governing boundary layer equation for fluid flow through a porous medium by using a generalized

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = \frac{\partial^2 u}{\partial y^2} + \frac{\epsilon \mathbf{n}_x}{K} (u_\infty - u) + c \epsilon^2 (u_\infty^2 - u^2) \quad (1)$$

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \quad (2)$$

Where  $u, v$  are the velocity components in the  $x, y$  direction, respectively, and  $K$  are the porosity and the permeability of the porous medium,  $\nu$  the kinematic viscosity,  $\nu_e$  the effective kinematic viscosity.

### 3- Boundary conditions

As for the surface roughness of the plate, we shall assume the slip velocity  $u_s$  to be proportional to the gradient of the velocity  $u$  at the wall. The condition to be considered is

$$u_s = R \frac{\partial u}{\partial y} \quad (3)$$

at the plate ( $y = 0$ )

The proportionality factor  $R$  is approximately the height of the roughness element, and is taken to be of the same order of magnitude as the boundary layer thickness  $\mathbf{d}$ . In other words from the model assumed in equation (3), we can write

$$\frac{u_s}{u_\infty} \cong \frac{R}{\mathbf{d}}$$

In our calculations we shall take  $R \cong O\left(\frac{\mathbf{d}}{10}\right)$  which seems to be practically reasonable even for extremely smooth surfaces.

The boundary conditions for our problem are then given by:

$$\begin{aligned} y=0: \quad u &= R \frac{\partial u}{\partial y}, \quad v=0 \\ y \rightarrow \infty: \quad u &= u_\infty \end{aligned} \quad (4)$$

A stream function of the form  $\mathbf{y} = \sqrt{2u_\infty \nu x} f(\mathbf{h})$  where  $f(\mathbf{h})$  denotes the dimensionless stream function and  $\mathbf{h} = \sqrt{\frac{u_\infty}{2\nu x}} y$  is introduced to satisfy the continuity equation (2). The expressions for  $u$  and  $v$  are

$$u = u_\infty f'(\mathbf{h}), \quad v = \sqrt{\frac{\nu u_\infty}{2x}} [-f(\mathbf{h}) + \mathbf{h} f'(\mathbf{h})]$$

Where prime denotes differentiation with respect to  $\mathbf{h}$ , and for the roughness parameter

$$R_w = \frac{R(x)}{u_\infty} \sqrt{\frac{u_\infty}{2\nu x}} \text{ is constant, (hence } R(x) \sim x^{-1/2} \text{ for similarity solution).}$$

Substitution in equation (1) and simplification leads to the following non-linear ordinary differential equation:

$$f''' + f f'' + M(1 - f') + N(1 - f'^2) = 0, \quad (5)$$

Where  $M = \frac{2 \epsilon x}{Ku_\infty}$  (permeability parameter),

$N = 2c \epsilon x$  (Inertia coefficient parameter).

The boundary condition now become.

$$y=0: f' = R_w f', \quad f = 0 \quad (6)$$

$$y \rightarrow \infty: f' = 1$$

#### 4- Numerical Solution And Discussion

Equation (5) with the boundary conditions (6) are solved numerically using the shooting method, with the fourth order Runge-kutta.

For engineering application, the local wall shear stress is of importance. The shear stress.

$$\tau_w = \mu_\infty \sqrt{\frac{u_\infty}{2x}} f''(0) \quad (7)$$

At the plate the coefficient of skin friction  $C_f$  is given by

$$C_f = \frac{\tau_w}{\frac{1}{2} \rho u_\infty^2} = \sqrt{2} R_x^{-1/2} f''(0) \quad (8)$$

$$\text{where } R_{ex} = \frac{\rho u_\infty x}{\mu}$$

Figure 1 displays the effect of the permeability parameter  $M$  on the distribution of velocity within the boundary layer. The results indicate that the velocity increases as  $M$  increases.

Figure 2 shows the results for the velocity distributions in the boundary layer. As the coefficient of inertia parameter  $N$  increases, we observe that the velocity increases.

Figure 3 represents the distributions of the velocity within the boundary layer. It is found that the velocity increases with increasing the roughness parameter  $R_w$ .

From the numerical results obtained in Table 1, it is observed that:

- (a)  $C_f$  decreases with the increasing values of  $R_w$  while  $N$  and  $M$  are kept constants.
- (b)  $C_f$  increases with the increasing values of  $M$  while  $N$  and  $R_w$  are kept constants.
- (c)  $C_f$  increases with the increasing values of  $N$  while  $M$  and  $R_w$  are kept constants.

Table 1: Summary of our numerical results for  $f''(0)$

M	N	$R_w = 0$	$R_w = 0.05$	$R_w = 0.1$	$R_w = 0.15$
0.5	0.1	0.90984	0.880226	0.851642	0.824059
1	0.1	1.14892	1.09587	1.04652	1.00066
2	0.1	1.52077	1.42187	1.33401	1.25561
0.5	0.3	1.044	1.00471	0.966987	0.930956
1	0.3	1.25873	1.19609	1.13804	1.08434
2	0.3	1.6058	1.49754	1.40151	1.31604
0.5	0.5	1.16342	1.11446	1.06776	1.02349
1	0.5	1.35991	1.28773	1.22107	1.15966
2	0.5	1.6866	1.56899	1.46486	1.3724

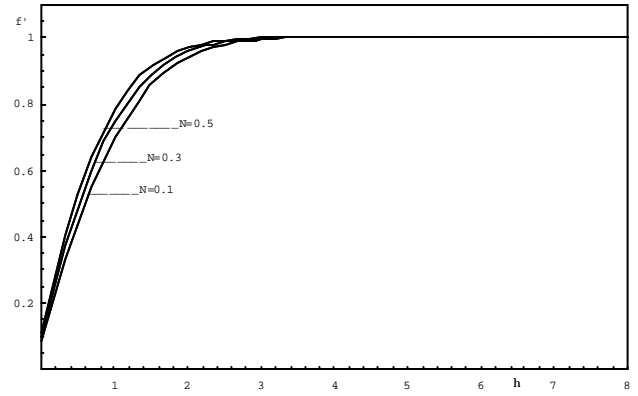


Figure2. velocity profiles for various values of  $N$  at  $M=0.5$  and  $R_w=0.1$

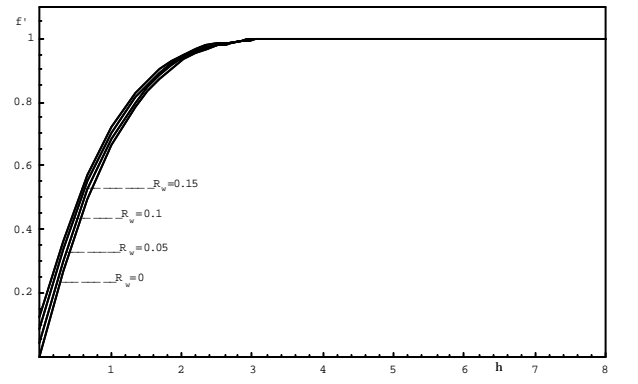


Figure3. velocity profiles for various values of  $R_w$  at  $N=0.1$  and  $M=0.5$

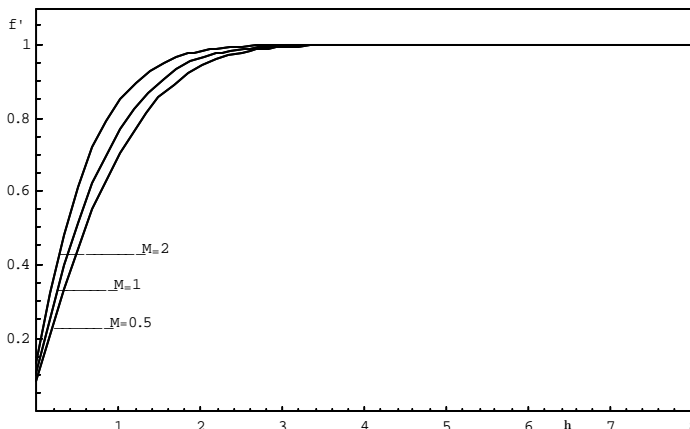


Figure1. Velocity profiles for various values of  $M$  at  $N=0.1$  and  $R_w=0.1$

## *References*

- [1] Vafai, K.; Tien, C.L.:  
effects on flow and heat transfer in  
porous media, *Int. J. Heat Mass  
Transfer* 24,1981, 195-203.
- [2] Plumb, O.A.; Huenefeld, J.C. -Darcian  
natural convection from heated surfaces  
*J. of  
Heat Mass Transfer* 24,1981, 765-768.
- [3] Vafai.; Tien, C.L.  
effects on convective mass transfer in  
*transfer*, 1982,1183-1190.
- [4] Yang, J.; Shiang, C.T.  
convection plume along a vertical  
adiabatic surface embedded in a non-  
*nt. J. Heat  
Mass transfer* 40 (7),1997, 1693-1699.
- [5] Kaviany; M.  
forced convection heat transfer from a  
semi-infinite flat plate embedded in  
*Journal of Heat  
transfer* vol. 109/345,1987.
- [6] Schlichting  
*Graw-Hill Book C.D.*, New York, 551,  
1960.

