

# Specific peculiarities of the jets penetrating the liquid pool of different density under severe accidents at the NPP conditions and their modeling and simulation

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**Abstract:** - The paper is devoted to one of the problems of the modelling and simulation of the severe accidents at the nuclear power plants (NPP) in touch with development and operation of the passive protection systems against severe accidents. The results of the mathematical modelling and simulation of the jets penetrating the pool of other liquid under diverse conditions as well as an analysis of the experimental data have clearly shown that the falling buoyant jets penetrating the pool of other liquid differ a lot from the classical jets moved by pressure gradient. For example, the classic scheme with monotone jet radius evolution does not work in this case. There is clearly observed phenomenon that jet is going with nearly constant radius up to some point in a pool, then at the point of "bifurcation" it substantially changes its radius abruptly (jet switches its one constant radius to the another one). These specific peculiarities of the penetrating jets are discussed and mathematical modelling of the problem is considered.

**Key-Words:** - Jet, Penetration, Pool, Bifurcation, Mathematical Modelling, Non-linear Phenomenon, Switch of Radius, Passive Protection System.

## 1 Introduction

Peculiarities of the penetration dynamics of a liquid jet into the other liquid medium have been studied in a number of papers [1-15]. Most of the earlier studies have been performed in the metal and nuclear industries, e.g. [1, 4-7, 9-11]. But the problem still remains, especially in the case of the thick jets when they are penetrating a pool of other liquid without disintegration and in case of dominated inertia, drag and buoyancy forces. For the thin jets it has been shown [16] that the jet instability might be caused by the bending perturbations of its axis.

The objective of present paper is determining the penetration behaviours of a thick jet into a fluid pool and analysis of the phenomenon that jet is going with nearly constant radius up to some point in a pool, then at the point of "bifurcation" it substantially changes its radius abruptly (jet switches its one constant radius to the another one) as illustrated by experimental data borrowed from [17] shown in Fig. 1. Numerical simulation was performed with the computer code Casper [17].

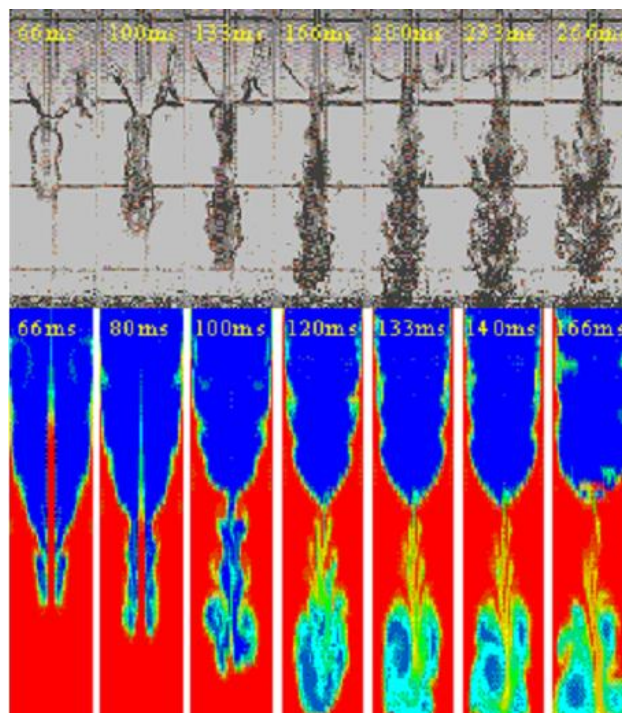


Fig.1. Jet penetration features: experimental and numerical data (initial velocity of the jet was 4m/s)

Both data, experimental and numerical, for further support of the above-mentioned peculiarities of a jet penetration into a pool are presented in the pictures in Fig.2 for the corresponding moments of time (in ms):



Fig.2. Features of a jet penetration into the pool: experimental data for initial velocity 4m/s, 6m/s, 9m/s, respectively (from the top to the bottom)

This contradicts to the classic jet scheme when jet is considering as gradually changing its radius due to the losses of the velocity [2, 18]:

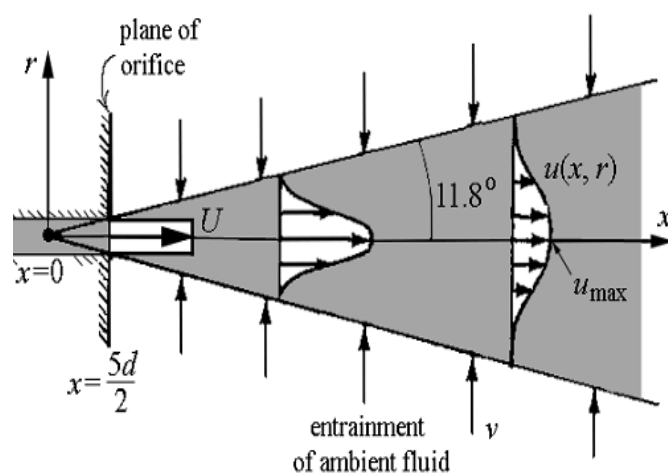


Fig.3. Schematic description of a jet penetrating in a fluid at rest

The widening is linear with distance, and all cross-jet velocity profiles, except those very near the orifice, are similar to one another, after suitable averaging over turbulent fluctuations. Similar schematic representations were considered for the laminar jets as well.

This corresponded very well to a huge number of experimental data, e.g. shown in Fig. 4 for the jet injected to the melt pool from the orifice under the layer of the melt [19].

## 2 The non-linear isothermal model of a jet penetration into the liquid pool of other density

### 2.1 Jet penetration into another liquid at the non-boiling and isothermal conditions

To analyze the penetration phenomena of a plunging jet into another liquid with various densities a non-linear analytical and numerical models and CFD simulations based on the developed algorithms were developed both at the non-boiling and isothermal conditions, as well as at the boiling and non-isothermal conditions. The results were compared with a series of visualization tests. In the tests a 10 mm water jet with an injection velocity up to 9 m/s plunges on to a liquid with various densities. The general behaviours of the plunging jet consists of surface cavity of a pool liquid by the initial impact of the jet, air pocket formation during the

penetration, radial bottom spreading of the jet and entrained air and interfacial instability between the pool liquid and entrained air.



Fig.4. Experimental data by jet injection

The analytical solutions for continuous and finite jets are reasonably described the characteristics of the penetration behaviours. The numerical model is able to simulate these general behaviours of the plunging jet and provides reasonable match on the penetration velocities.

It is clearly observed that the penetrating jet is going first with approximately stable radius and then is changing its radius abruptly to another bigger one. This bifurcation point is explained from the analytical solution obtained below.

## 2.2 Basic assumptions of the mathematical model

The jet penetrating the pool is supposed as a body of a variable mass assuming that the jet is moving under an inertia force acting against the drag and buoyancy forces. The surface forces are supposed to be negligible comparing to the three above-mentioned ones.

A radius of the jet is assumed to be approximately constant during the jet penetration or at least during some part of the length of penetration. This allows calculating the jet penetration process step-by-step in a general case taking first the constant jet radius, then the other one constant jet radius, and so on. Thus, the equation of a jet momentum considering a jet as a body of a variable mass is written as follows:

$$\rho_1 \frac{d(hv_1)}{dt} = h(\rho_1 - \rho_2)g - \frac{1}{2} \rho_2 v_1^2, \quad (1)$$

where  $h$  is the length of a jet penetration into the pool,  $\rho_1, \rho_2$  are the densities of the jet and fluid in the pool, respectively,  $v_1$  is the jet velocity. Obviously here is  $v_1 = dh/dt$ .

For the thick jets, which are not prone to the bending instabilities (say, their radius is of the same order as their length of penetration) we can neglect surface forces retaining the only drag force together with the buoyancy and inertia forces.

## 2.3 Dimensionless mathematical model

In a general case of different densities of a jet and a pool when  $\rho_{12} = \rho_1 / \rho_2 \neq 1$ , the non-linear equation (1) may be transformed to the dimensionless form:

$$h \frac{d^2 h}{dt^2} + \left(1 + \frac{\rho_{21}}{2}\right) \left(\frac{dh}{dt}\right)^2 + \frac{\rho_{21} - 1}{Fr} h = 0, \quad (2)$$

where  $\rho_{21} = \rho_2 / \rho_1$ ,  $Fr = u_0^2 / (gr_0)$  is the Froude number, which characterizes the ratio of the inertia and buoyancy forces. Here the following scales were used for the velocity and for the time:  $u_0$  and  $r_0 / u_0$ , respectively.

It is clearly shown by equation (2), which can be treated as a mathematical model of the process, that the Froude number and the density ratio of the liquid in a pool and jet predetermine completely the process of a thick jet penetration into a pool. Let us remind ones more that the bending perturbations of the axis are not available for the thick jets in contrast to the thin jets [17].

The initial conditions for the jet momentum equation (2) are stated the next ones:

$$t = 0, \quad h = 0, \quad dh/dt = u_0, \quad (3)$$

where  $u_0$  is the initial velocity of a jet before its penetration into the pool.

#### 2.4 Singularity of the initial conditions and their treatment

The initial conditions (3) contain singularity due to difference of the jet and pool velocities at their contact area at the first moment ( $t=0$ ). A jet has velocity  $u_0$ , while a pool is in the rest before contact ( $h=0$ ) changing its velocity at the moment of contact from 0 to  $u_0$ . In fact, velocity  $u_0$  is going to change (decrease) due to a contact of a jet and a pool. If the dissipation energy is neglected, then an initial velocity is  $u_0$  but might cause big inaccuracy in a solution of a problem.

To avoid singularity of the initial conditions (3), the following initial conditions might be considered instead of the above-mentioned initial conditions:

$$t = 0, \quad h = h_0, \quad dh/dt = u_p, \quad (4)$$

where  $h_0$  and  $u_p$  are the initial length and velocity of a jet penetration (after a first contact of a jet with a pool). The equation (2) is solved with the initial conditions (4), where  $h_0$  and  $u_p$  are computed using the Bernoulli equation and the jet momentum equation in the form:

$$0.5\rho_1 u_0^2 = 0.5\rho_1 u_p^2 + (\rho_1 - \rho_2)gh_0 / u_0^2 - 0.5\rho_2 u_p^2, \quad (5)$$

$$\rho_1 H u_0 = \rho_1 H u_p + \rho_2 h_0 u_p,$$

where  $H$  is the initial length for the finite jet falling into the pool. In case of a jet spreading out of a nozzle (not a jet of the finite length), this value is determined by a pressure at the orifice outlet as shown in Fig. 2.

Solution of the equation array (5) is presented in a dimensionless form as follows

$$h_0 = \frac{H}{\rho_{21}} \left( \frac{\sqrt{1 + \rho_{21}}}{\sqrt{1 + 2(1 - \rho_{21})h_0 / Fr}} - 1 \right), \quad (6)$$

$$u_p = \sqrt{\frac{1 + 2h_0(1 - \rho_{21}) / Fr}{1 + \rho_{21}}}.$$

#### 2.5 Solution of the Cauchy problem for the mathematical model obtained

The Cauchy problem (2), (6) was solved with the special coupled transformations of the dependent and independent variables altogether:

$$h = \left( \frac{2A + 1}{2} \right)^{\frac{2}{2A+1}} X^{\frac{2}{2A+1}}, \quad (7)$$

$$dt = \left( \frac{1}{2A + 1} \right)^{\frac{1}{2A+1}} X^{\frac{1}{2A+1}} d\tau,$$

where  $A = 1 + \rho_{21}/2$ . Then using the equation (7) with a few further simple transformations yields the following linear second-order equation in the new variables:

$$\frac{d^2 y}{d\tau^2} + \frac{\rho_{21}^2 - 1}{2Fr^2} = 0.$$

Here  $y$  is a new variable stated by the equation  $X = e^y$ . Finally the solution is

$$y = c_1 e^{k\tau} + c_2 e^{-k\tau},$$

where  $c_1, c_2$  are the constants computed from the initial conditions (6). The eigen value  $k$  is

$$k = \sqrt{(1 - \rho_{21})[1 + 0.5(1 + \rho_{21})] / Fr}.$$

In case a pool is denser than a jet ( $\rho_{21} > 1$ ),  $k$  is an imaginary value, and the solution is

$$y = c'_1 \cos k\tau + c'_2 \sin k\tau.$$

### 3 The bifurcation of the penetrating jet and abrupt change of its radius

#### 3.1 Substantiation of the jet penetrating pool schematic with abrupt changes of its radius

The exact analytical solution thus obtained was based on the assumption about the constant jet radius; therefore it is strict for a solid rod penetration into the pool and for some initial part of a jet penetration before the remarkable growing of its radius. It might be used as approximate step-by-step solution for a jet penetration into a pool for small temporal intervals correcting the jet radius from one to another one.

It is highly important to estimate an evolution of the jet's radius to get support of the assumptions made or obtain an idea on how to correct solution in a good correspondence to the existing experimental data. For this the Bernoulli equation and the mass conservation equation are considered for the jet penetrating a pool as follows:

$$S_1((\rho_1 - \rho_2)hg + 0.5\rho_1v_1^2) = 0.5\rho_1u_0^2S_0, \quad (8)$$

$$\rho_1v_1S_1 = \rho_1u_0S_0.$$

Here  $S$  is the cross section area of the jet. Indexes 0 and 1 denote the initial state and the current state of the jet.

### 3.2 Dimensionless conservation equations for the jet

In a dimensionless form, retaining the same symbols, the equation array (8) yields:

$$S_1[2h(1 - \rho_{21})/Fr + v_1^2] = 1, \quad (9)$$

$$S_1v_1 = 1.$$

The equation array (9) has the following solution:

$$S_1 = \frac{Fr}{4h(1 - \rho_{21})} \left[ 1 \pm \sqrt{1 - 8h(1 - \rho_{21})/Fr} \right], \quad (10)$$

$$v_1 = 1/S_1$$

As follows from (10), both possible values of the jet radius are available. One is the initial jet radius while the other value means that jet may lose its stability and change the radius abruptly as we could see from the experimental data above.

### 3.3 Bifurcation of a jet

Thus, we have got quite unexpected result (10), where from follows that there are two available solutions for the jet radius, with the point of bifurcation, which depends on the Fourier number and density ratio as follows:

$$h = \frac{Fr}{8(1 - \rho_{21})}. \quad (11)$$

After the point of bifurcation (11) the solution (10) does not exist in real numbers, therefore the jet

can switch its radius abruptly between two available stable states.

The jet starts penetration into the pool with initial cross-sections, thus,  $S_1=1$ . Further analysis of the equation (11) shows that for a small penetration depth or, more generally, in case of

$$8h(1 - \rho_{21}) \ll Fr, \quad (12)$$

Solution (10) gives the following pair of the available jet radiuses to switch between them:

$$S_1 \approx 1, \quad (13)$$

$$S_1 \approx \frac{Fr}{2h(1 - \rho_{21})} \gg 1.$$

### 3.4 Specific features of the jet penetration

Thus, there is no reason for a jet to become abruptly from the section area 1 to the bigger one at the beginning of its penetration into a pool of other liquid because the jet momentum directs mainly along its axis. But then, with a jet further penetration into a pool, due to instability of a jet causing by its free surface perturbations and by a loss of momentum, the jet area may change at any moment.

Strictly saying, this phenomenon revealed by simple integral analysis requires complete investigation of the instability with the bifurcation analysis, therefore it is a subject of a separate paper. Here only some estimation is been done for the moment.

### 3.5 Calculation of the examples to illustrate the results obtained

Starting penetration into a pool from  $S_1=1$  the jet should become to a cross-section value  $S_1=2$  at the point

$$h_1 = \frac{Fr}{8(1 - \rho_{21})} = \frac{1}{8Ri},$$

when further existence of the two possible jet's radiuses is impossible. Here  $Ri = (1 - \rho_{21})/Fr$  is the Richardson number (the ratio between the momentum and the buoyancy forces of a jet).

The phenomenon of a jet penetration into a pool of other liquid accounting the results obtained and the experimental data presented above may be explained as follows. The jet penetrates into a pool at the distance  $h = h_0$  determined by the initial

length of a jet, the Froude number and the density ratio. In case of a long jet as well as the jet permanently spreading out of the nozzle the initial penetration length is determined by the Froude number and the density ratio. Then jet is going with an increase of its radius till  $h = h_1$ , which represents the bifurcation point. After this bifurcation point, the jet is abruptly switched and further goes with a nearly constant radius. Applying the solution obtained to those parts

with their own initial data, the whole jet might be computed based on the analytical solution obtained.

From the equation (13) a jet cross-section at the depth of penetration

$$h = h_0$$

is as follows:

$$S_1 = 0.5\rho_{12}(1 \pm \sqrt{1 - 4\rho_{21}})$$

where from for the density ratio 0.1 yield the following two available stable states of the jet:

$$S_1 \approx 1,15, r_1 \approx 1,07, v_1 \approx 0,87,$$

and

$$S_1 \approx 8,87, r_1 \approx 2,98, v_1 \approx 0,11,$$

where from one could see the approximate correspondence to the above experimental pictures.

## 4 The non-linear non-isothermal model of a jet penetration into the liquid pool of other density

### 4.1 Jet penetration into another liquid at the boiling and non-isothermal conditions

In many practical applications, for example during severe accidents at the nuclear power plants (NPP) the high-temperature corium melt jet is penetrating the pool of volatile coolant.

Then jet penetration into the coolant is going under the non-isothermal conditions and by action of the vapor flow against the jet. The schematic model for such case is presented in Fig.4. This model is taking into account the vapor pressure acting on the jet due to high temperature of the jet.

The other assumptions are similar to the previous model. The jet velocity is computed as  $V_1 = dx / dt$ , где  $x$  is coordinate from the pool surface into the pool by jet penetration,  $x = 0$  is the equation of the

pool free surface at the rest. The jet radius is  $a$ , the length is  $h$ , then the initial jet velocity is  $V_0$ .

### 4.2 Mathematical model of the jet penetrating pool of volatile coolant

Development of the model for the described system is based on the momentum conservation equation written in the following form:

$$\rho_1 h \frac{dV_1}{dt} = g(\rho_1 h - \rho_2 x) - \alpha \rho_2 V_1^2 - \beta \rho R T_1, \quad (14)$$

where the cross-sectional area multiplayer  $S_1 = \pi a^2$  is omitted. Here  $g$  acceleration due to gravity,  $h$  is the cylindrical jet length,  $\rho$  is the density of the vapor,  $T_1$  is the temperature of the vapor,  $R$ - universal gas constant,  $\alpha$ - drag force coefficient (depends on the jet form and flow regime).

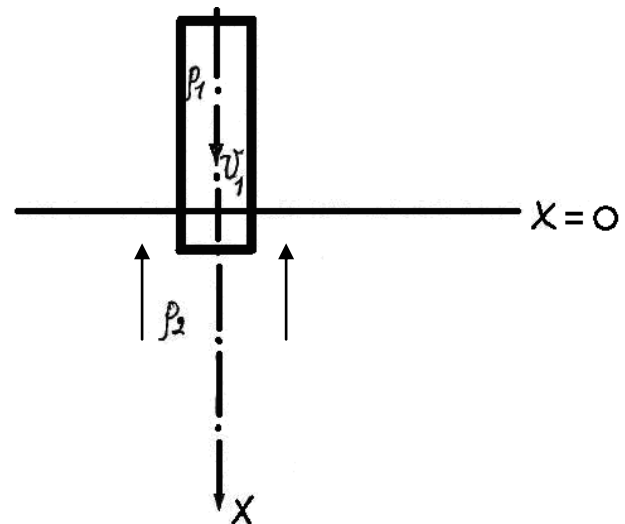


Fig.5. Schematic representation of the jet penetrating the pool of volatile coolant

We take the maximum value  $\alpha=0.5$  for conservative estimations,  $\beta$ - empirical constant to be computed from the experimental data (max  $\beta=1$ ).

### 4.3 The Cauchy problem for the equation of the jet penetration

The non-linear differential equation (14) with the initial conditions:

$$t=0, \quad x=0, \quad \frac{dx}{dt} = V_n, \quad (15)$$

where  $V_n=V_0$  for the thin jet and for the thick slow jets (or in a pool of small density), represent the Cauchy problem for this case.

The equation (15) is rewritten in the following form:

$$\frac{d^2x}{dt^2} + \alpha A \left(\frac{dx}{dt}\right)^2 + gAx + C = 0, \quad (16)$$

where  $A = \rho_{12}h$ ,  $C = b/h - g$ , with the  $x \geq h$  the  $Ax = \rho_{12} = const$ .

The time  $t$  as a variable is present in the equation (16) implicitly, therefore the equation is autonomous. By  $x \geq h$  the equation (16) transforms to

$$\frac{d^2x}{dt^2} + \alpha A \left(\frac{dx}{dt}\right)^2 + g\rho_{12} + C = 0, \quad (17)$$

#### 4.4 Analytical solution of the equation array

The second-order non-linear differential equation (17) has analytical solution. For this, the equation better to transform to the dimensionless form, which is preferable in many cases as the most general one.

Thus, the Cauchy problem (17), (15) is transformed to a dimensionless form with the characteristic velocity  $V_0$ , characteristic distance  $a$ , and time  $a/V_0$ . Then dimensionless form of the above equation is getting the next form:

$$\frac{d\bar{x}}{d\bar{t}} = \bar{v}, \quad (18)$$

$$\frac{d\bar{v}}{d\bar{t}} = - \left[ \varepsilon \alpha \rho_{21} \bar{v}^2 + \frac{1}{Fr^2} (x \varepsilon \rho_{21} + \bar{b} - 1) \right],$$

$$\bar{x} \leq 1/\varepsilon;$$

$$\bar{t} = 0, \quad \bar{x} = 0, \quad \bar{v} = \bar{v}_n, \quad (19)$$

where the last term in a second equation (18) by  $\bar{x} > 1/\varepsilon$  is equal to  $(\rho_{21}-1)/Fr^2$ ,  $Fr^2 = V_0^2 / (ga)$  – the Froude number,  $\varepsilon = a/h$  – the ration of the radius and the length of the round jet,  $\bar{b} = n/V_0^2$  – ratio of the vapor potential energy and kinetic energy of the jet,  $\bar{v}_n = 1$ , or  $\bar{v}_n = 1 - 4\varepsilon\rho_{21}/(3\pi)$  if the shock of the jet and free surface of the rest pool is accounted.

General view of the autonomous equation array (18) has the next form

$$\frac{dx}{dt} = V, \quad (20)$$

$$\frac{dV}{dt} = -(\alpha AV^2 + gAx + C),$$

where from follows that velocity of the penetrating jet tends to falling with time, except the case  $Ax < 1$ , or  $x < h\rho_{12}$ , which corresponds to the initial stage of the jet penetration when

$$\alpha AV^2 + g(Ax - 1) + b/h < 0,$$

or

$$V^2 < gh(1 - \rho_{21}) - b, \text{ by } x \geq h;$$

and

$$V^2 > gh(1 - \rho_{21}) - b, \text{ by } x < h,$$

where from seen that by substantially big influence of the vapor flow on a jet penetration this case is impossible, because otherwise it requires:

$$gh(1 - \rho_{21}) > b, \text{ by } x \geq h$$

or

$$g(h - \rho_{21}x) > b, \text{ by } x < h.$$

The mathematical model thus developed is applied for simulation of the corium jet penetrating the pool of volatile coolant under reactor vessel at NPP in the passive protection systems against severe accidents at NPP. For this, the dimensionless form (18), (19) and dimension forms (20) or (15)-(17) are applied.

#### 4.5 Dimensionless analytical solution

With account of the above-mentioned, the analytical solution for the equation array (18) is got as follows:

$$\bar{x} = \frac{1}{\alpha \rho_{21} \varepsilon} \ln \left| \cos \left[ \frac{1}{Fr} \sqrt{\frac{\rho_{21} - 1 + \bar{b}}{\alpha \rho_{21} \varepsilon}} (\bar{c}_1 + \dots) \right] \right| + \bar{d}_1, \quad (21)$$

$$\bar{v} = \frac{1}{Fr} \sqrt{\frac{\rho_{21} - 1 + \bar{b}}{\alpha \rho_{21} \varepsilon}} \operatorname{tg} \left[ \frac{1}{Fr} \sqrt{\frac{\rho_{21} - 1 + \bar{b}}{\alpha \rho_{21} \varepsilon}} (\bar{c}_1 + \dots) \right],$$

$$\rho_{21} > 1 - \bar{b};$$

$$\bar{x} = \frac{1}{\alpha\rho_{21}\varepsilon} \ln \left| \exp \left[ \frac{1}{Fr} \sqrt{\frac{1-\rho_{21}-\bar{b}}{\alpha\rho_{21}\varepsilon}} (\bar{c}_2 - \alpha\rho_{21}\varepsilon\bar{t}) \right] - \exp \left[ \frac{1}{Fr} \sqrt{\frac{1-\rho_{21}-\bar{b}}{\alpha\rho_{21}\varepsilon}} (\alpha\rho_{21}\varepsilon\bar{t} - \bar{c}_2) \right] \right| + \bar{d}_2, \tag{22}$$

$$\bar{v} = -\frac{1}{Fr} \sqrt{\frac{1-\rho_{21}-\bar{b}}{\alpha\rho_{21}\varepsilon}} * \text{cth} \left[ \frac{1}{Fr} \sqrt{\frac{1-\rho_{21}-\bar{b}}{\alpha\rho_{21}\varepsilon}} (\bar{c}_2 - \alpha\rho_{21}\varepsilon\bar{t}) \right],$$

$$\rho_{21} < 1-\bar{b}, \quad \bar{v} > \frac{1}{Fr} \sqrt{\frac{1-\rho_{21}-\bar{b}}{\alpha\rho_{21}\varepsilon}};$$

$$\bar{x} = -\frac{1}{\alpha\rho_{21}\varepsilon} \ln \left| \exp \left[ \frac{1}{Fr} \sqrt{\frac{1-\rho_{21}-\bar{b}}{\alpha\rho_{21}\varepsilon}} (\bar{c}_3 + \alpha\rho_{21}\varepsilon\bar{t}) \right] + \exp \left[ -\frac{1}{Fr} \sqrt{\frac{1-\rho_{21}-\bar{b}}{\alpha\rho_{21}\varepsilon}} (\bar{c}_3 + \alpha\rho_{21}\varepsilon\bar{t}) \right] \right| + \bar{d}_3, \tag{23}$$

$$\bar{v} = -\frac{1}{Fr} \sqrt{\frac{1-\rho_{21}-\bar{b}}{\alpha\rho_{21}\varepsilon}} \text{th} \left[ \frac{1}{Fr} \sqrt{\frac{1-\rho_{21}-\bar{b}}{\alpha\rho_{21}\varepsilon}} (\bar{c}_3 + \alpha\rho_{21}\varepsilon\bar{t}) \right],$$

$$\rho_{21} < 1-\bar{b}, \quad \bar{v} < \frac{1}{Fr} \sqrt{\frac{1-\rho_{21}-\bar{b}}{\alpha\rho_{21}\varepsilon}}.$$

Here are:  $\bar{c}_{1-3}, \bar{d}_{1-3}$  - constants to be computed from the initial conditions (19),  $\bar{b} = b/(hg)$ .

## 5 Study of the non-linear non-isothermal model of a jet penetration into the liquid pool of other density

### 5.1 Peculiar point of the equation array

The equation array (18) has peculiar point

$$\bar{x}_0 = (1-\bar{b})\rho_{12} / \varepsilon, \quad \bar{v}_0 = 0,$$

which is for the jet without vaporization:

$$\bar{x}_0 = \rho_{12} / \varepsilon, \quad \bar{v}_0 = 0.$$

But as far as (18) satisfies at the interval  $\bar{x} \leq 1/\varepsilon$ , the peculiar point belongs to the determination region:

$\rho_{21} \geq 1-\bar{b}$ , what corresponds to the solution (21) after point  $\bar{x}=1/\varepsilon$ .

If  $\rho_{21} < 1-\bar{b}$ , then a peculiar point is absent and solution after the point  $x=1/\varepsilon$  has the form (21) or (22) depending on the velocity of a jet penetration

into a pool. A jet moves until the point  $\bar{x}=1/\varepsilon$  without any peculiarities and continues its

movement after the point  $\bar{x}=1/\varepsilon$  in accordance with the solution (21)-(23) thus obtained.

In a peculiar point  $\bar{x}=x_0$  the jet velocity becomes zero (jet stops – does not exist anymore as a jet or continues its movement if it is denser jet than a pool, due to gravitation).

The maximal penetration length of a jet into a pool by  $m < 0$  (jet velocity decreases with  $\bar{x}$ ) is the same as by  $m > 0$  (jet velocity increases with  $\bar{x}$ ). The difference is only that in a first case  $\bar{V}_* > 0$  (jet is moving in a pool downwards), while in a second case  $\bar{V}_* < 0$  (jet moves in the opposite direction – vertically up in a pool). Thus, a jet decelerates until the point of a rest and then moves up, or it stops at the point  $\bar{x} = \bar{x}_*$  ( $\bar{V}_* = 0$ , by  $m=0$ ).

In an absence of vaporization in a pool ( $\bar{b}=0$ ), the peculiar point is absent if pool is lighter than a jet (or penetrating a pool solid body). The peculiar point is moving inside the pool (the jet penetration length is growing) with decrease of a jet radius and density ration of the pool and jet.

Vaporization in a pool decreases this critical level up to zero value, and available even shock due to a vapor explosion,  $\bar{b} > 1$ .

### 5.2 Phase trajectories of a jet

The second equation of the equation array (18) may be divided by the first one and get the following equation for the phase trajectories of the system:

$$\frac{d\bar{v}}{d\bar{x}} = -\frac{\varepsilon\alpha\rho_{21}Fr^2\bar{v}^2 + \varepsilon\rho_{21}\bar{x} + \bar{b} - 1}{Fr^2\bar{v}}, \tag{24}$$

with the boundary conditions:



$$\bar{x} = 0, \quad \bar{v} = \bar{v}_n. \quad (25)$$

The first-order differential equation (24) determines for each point  $(\bar{x}, \bar{v})$  the corresponding direction of the going through it curve  $d\bar{v}/d\bar{x}$ . Thus, a field of such directions («portrait» of the differential equation on a phase plane) allows producing a sketch  $\bar{v}(\bar{x})$  and then determine the solution of the equation by the stated initial values of the  $\bar{x}$  and  $\bar{v}$ . Let us start from the points of constant jet velocity directions  $d\bar{v}/d\bar{x} = m$  (isoclines, or the lines of the equal jet velocity gradients).

According to the above stated:

$$\varepsilon\alpha\rho_{21}Fr^2\bar{v}^2 + mFr^2\bar{v} + b + \varepsilon\rho_{21}\bar{x} - 1 = 0,$$

where from

$$\bar{v}_{1,2} = \frac{-mFr \pm \sqrt{m^2Fr^2 - 4\varepsilon\alpha\rho_{21}(b + \varepsilon\rho_{21}\bar{x} - 1)}}{2\varepsilon\alpha\rho_{21}Fr}. \quad (26)$$

Following the (26), one can get the condition for real jet velocity (real  $\bar{v}$ ):

$$\bar{x} \leq \bar{x}^* = \frac{\rho_{12}}{\varepsilon} \left(1 + \frac{m^2Fr^2}{4\alpha\varepsilon} \rho_{12} - \bar{b}\right) = \bar{x}_0 + \frac{m^2Fr^2}{4\alpha\varepsilon^2} \rho_{12}^2. \quad (27)$$

The equation (27) forecasts the maximal available length of a jet penetration into a pool by all possible parameters of the system of study. By  $m=0$  for example (zero gradient, jet is moving with constant speed by  $\bar{x}$ ) yields  $\bar{x}^* = \bar{x}_0$ .

The phase trajectories of a jet are illustrated in Fig. 6. There are available the following situations:

- $\rho_{21} \geq 1 - \bar{b}$ , the peculiar point is inside the definition region of the equations (18),  $\bar{x}_0 < 1/\varepsilon$ , and a jet can reach maximal penetration length ( $\bar{x}^* \leq 1/\varepsilon$ ) or continue its movement inside the pool according to the equations (21)-(23), if  $\bar{x}^* > 1/\varepsilon$ ;

- $\rho_{21} < 1 - \bar{b}$ , the peculiar point is outside the definition region of the equations (18) ( $\bar{x}_0 > 1/\varepsilon$ , and by  $\bar{x}^* > 1/\varepsilon$  even stronger than previous condition), therefore a jet moves until the point  $\bar{x} = 1/\varepsilon$  without any peculiarities and continues movement after the point  $\bar{x} = 1/\varepsilon$  according to the equations (21)-(23).

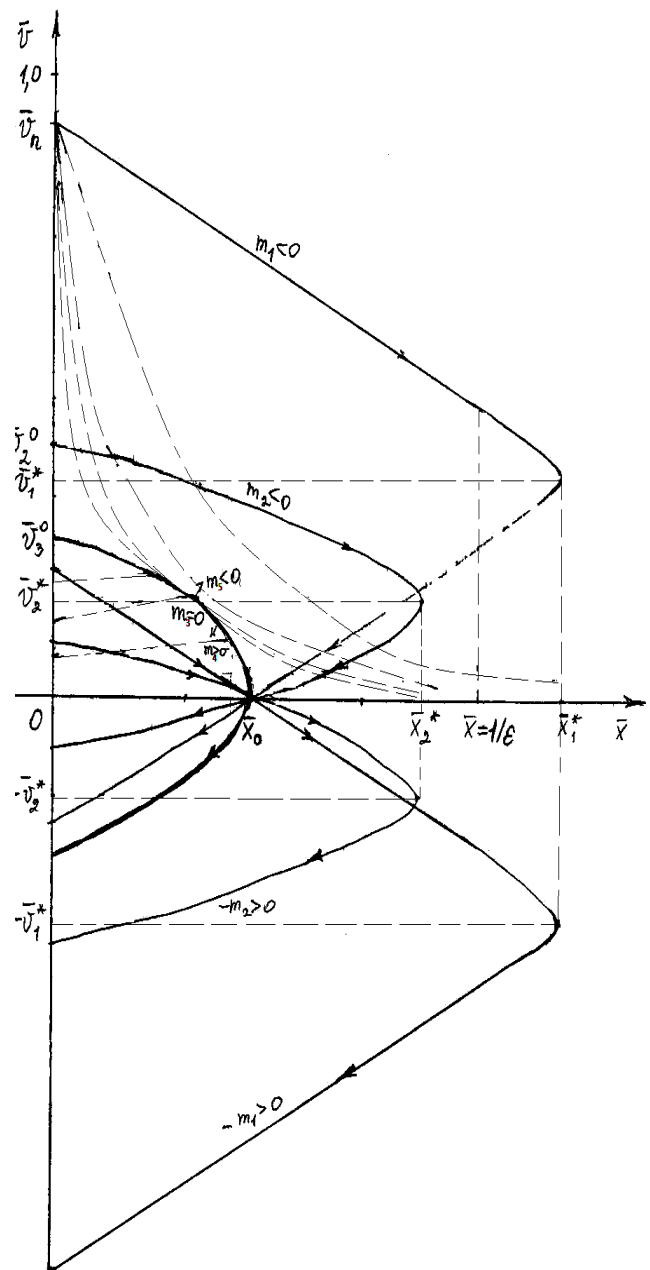


Fig.6. Phase portrait of a jet penetrating pool of volatile coolant

In a peculiar point  $\bar{x} = x_0$  jet velocity equal zero and it stops.

### 5.3 Vapor explosion in a pool

In case of a vapor explosion in a pool (big difference in a temperature between a jet and a pool determines the process together a heat capacity factor) the jet penetration length may be short. One can estimate it by the initial maximal velocity gradient when a jet just starts to penetrate the pool:

$$m_0 = -\frac{\alpha\varepsilon\rho_{21}\bar{V}_n^2 Fr^2 + \bar{b} - 1}{Fr^2\bar{V}_n}, \quad (28)$$

Then by  $\bar{b}_* = 1 + \alpha\varepsilon\rho_{21}\bar{V}_n^2 Fr^2$  a jet cannot penetrate a pool at all and with account of a shock on pool surface yields:

$$\bar{b}_* = 1 + \alpha\varepsilon\rho_{21} Fr^2 \left(1 - \frac{4\varepsilon}{3\pi} \rho_{21}\right)^2, \quad (29)$$

For a thin jet and low density of a pool (more generally,  $\varepsilon\rho_{21} \ll 1$ ) the equation (29) results in  $\bar{b}_* = 1 + \alpha\varepsilon\rho_{21} Fr^2$ , which means by low jet velocity when  $Fr^2 \sim 1$  or  $Fr^2 \ll 1$  that a jet weight is equalized by the vapour pressure. By  $Fr^2 \gg 1$  the value of  $\bar{b}_*$  may substantially prevail unite.

### 5.4 Numerical simulation of the system on computer

Some results of a computer simulations for the phase trajectories of a jet penetration into a pool of volatile coolant by the mathematical model developed were presented in Fig.6.

Let us analyze the results more in deep. The phase trajectories were presented for the next conditions:

$$\begin{aligned} m_1 &= \left(\frac{d\bar{V}}{d\bar{x}}\right)_{\bar{x}=0} < 0, \quad m_2 < 0, \quad m_2 > m_1, \\ m_3 &= 0, \quad m_4 > 0, \quad m_4 = -m_2, \\ m_5 &> 0, \quad m_5 = -m_1, \end{aligned}$$

$\bar{x}^*$  is a maximal jet penetration into a pool and  $x_0$  is a such critical point that all the trajectories (all isoclines) are going through it up to a point of the jet rest.

A peculiarity of the results obtained, as shown in Fig.6, is symmetry of the phase portrait with regards to an axis  $x$  for the same values of the parameter  $m$  of the opposite signs. The trajectory for  $m=0$  is symmetrical regarding the axis  $x$ . Dashed lines depict trajectories of a jet for different available conditions of its penetration into a pool. An interesting peculiarity is that none of the jet trajectories goes through the phase trajectory  $m=0$ , independently of the starting jet penetration velocity (initial jet velocity gradient  $m$ ).

### 5.5 Specific features of the results obtained

Despite a remarkable number of the papers done on a subject [20-31], the results obtained revealed some special features of a jet penetration into a pool, which may be of interest for the experts, both theoretical and experimental one.

## 6 Conclusion

The jet penetrating a pool of other liquid was investigated for different conditions. The problem is of interest for modelling and simulation of the severe NPP accidents in touch with development and operation of the passive protection systems. Analyses on the penetration phenomena of a jet into another liquid at the isothermal and non-isothermal conditions were performed and compared to the data from literature. The non-linear analytical models for the jet to predict the maximum penetration into a pool were developed and reasonably described the characteristics of the penetration behaviours.

The results of the mathematical modelling and simulation of the jets penetrating the pool of other liquid under diverse conditions as well as an analysis of the experimental data have clearly shown that the falling buoyant jets penetrating the pool of other liquid are quite different from the classical jets going under pressure gradient. For example, the classic scheme with monotone jet radius evolution does not work in this case. There is clearly observed phenomenon that jet is going with nearly constant radius up to some point in a pool, then at the point of "bifurcation" it substantially changes its radius abruptly (jet switches its one constant radius to the other one). These specific peculiarities of the penetrating jets were discussed and explained.

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